

Compositions Summary

Sampling

Fluid Initialization

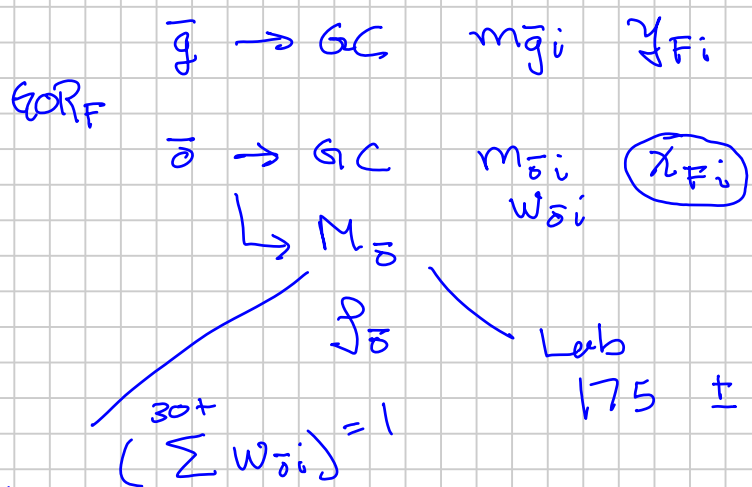
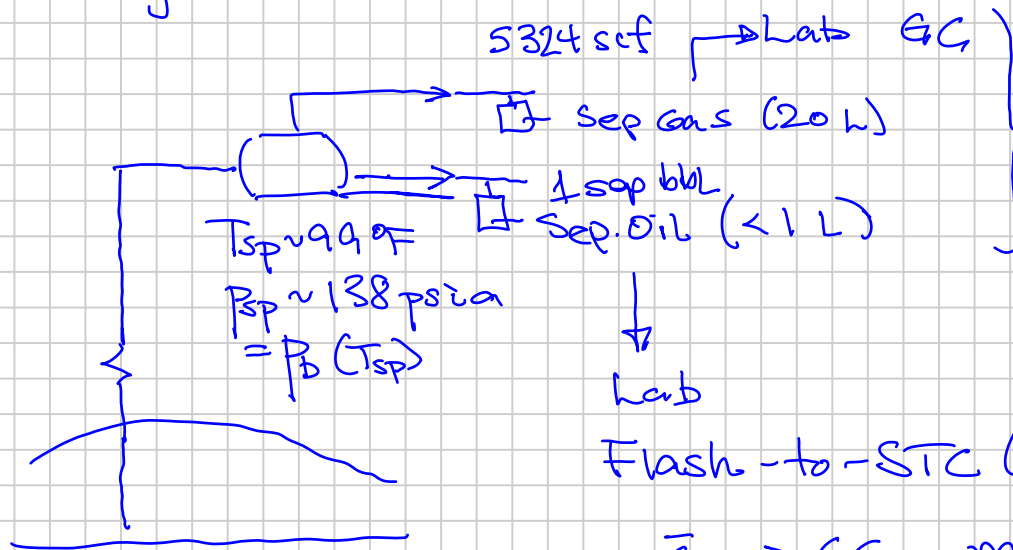
$Z_i \Leftrightarrow$

GOR

OGR

Product Ratios

(Bilal) Dynamite Gas Condensate (Sep. Sample)



Calc

$$M_{\bar{o}} = \frac{\sum_{i=1}^{30+} w_{oi} \pm}{\sum_{i=1}^{30+} \frac{w_{oi} \pm}{M_i \pm}}$$

± 165

$$M_{030+} = m_{\bar{0}} - \sum_{i=1}^{29} m_{\bar{0}i}^{GC}$$

- o Base-line Shift \pm
- o Internal Standard

$$A_i^{GC} \sim m_i^{GC}$$

$$GOR_{sp} = R_{sp} = \frac{scf}{sep. bbl} = 5324 \text{ scf/sep-bbl}$$

$$\Rightarrow f_{gsp}$$

$$z_{wi} = f_{gsp} y_{spi} + (1 - f_{gsp}) x_{spi}$$

e.g. C_1 67.227 75.480 3.099

$$\text{Back-Calc. } f_{gsp} = \frac{z_{wi} - x_{spi}}{y_{spi} - x_{spi}}$$

$$f_{gsp} = \frac{n_{gsp}}{n_{gsp} + n_{osp}}$$

$$= GOR_{sp}, \dots$$

$$\checkmark GOR_{sp} = \frac{V_{gsp}}{V_{osp}}$$

$$\frac{V_g}{n} = 379$$

$$pV_{sc} = nRT_{sc}$$

$$n_{gsp} = V_{gsp} \cdot \left(\frac{RT_{sc}}{p_{sc}} \right)^{-1}$$

Convert scf to lb-mole

$$\frac{1}{379} \frac{\text{lb-mole}}{\text{scf}}$$

$$n_{\text{osp}} = V_{\text{osp}} \cdot \left(\frac{P_{\text{osp}}}{M_{\text{osp}}} \right)$$

$$\equiv V_{\text{osp}}$$

Basis of $V_{\text{osp}} = 1 \text{ sep. lbl}$ (arbitrary) $\Rightarrow V_{\text{osp}} = 60 R_{\text{sp}}$

$$f_{\text{gsp}} = \frac{(1) R_{\text{sp}} / 379}{(1) R_{\text{sp}} / 379 + (1 \text{ lbl} \cdot 5.615 \frac{\text{ft}^3}{\text{lbl}}) \frac{P_{\text{osp}} \text{ (atm ft}^3)}{M_{\text{osp}} \left[\frac{\text{lb}}{\text{lb-mole}} \right]}}$$

$$f_{\text{gsp}} = \left\{ 1 + \frac{379(5.615)}{R_{\text{sp}}} \left(\frac{P_{\text{osp}}}{M_{\text{osp}}} \right) \right\}^{-1}$$

$$f_{\text{gsp}} = 0.768 \frac{\text{glcc}}{\text{glcc}} = \frac{47.9 \text{ lbl ft}^3}{\cdot} \times 62.4 \frac{\text{lbl ft}^3}{\text{glcc}}$$

$$M_{\text{osp}} = \underline{153.45} \text{ (calc'd } \pm)$$

$$f_{\text{gsp}} = \left\{ 1 + 379(5.615) \left(\frac{47.9}{153} \right) \left(\frac{1}{53.24} \right) \right\}^{-1}$$

$$= \underline{0.889} \quad \text{vs} \quad \underline{0.886}$$

vs. (using z_{wci} , y_{spci} , x_{spci})

e.g. c_1 67.227

$\frac{75.480}{\checkmark}$

$\frac{3.099}{\checkmark}$

Back-Calc. $f_{gsp} = \frac{z_{wi} - x_{spi}}{y_{spi} - x_{spi}}$

z_{wg} if $M_{osp} = 163 \Rightarrow f_{gsp}$
 \downarrow
 z_{wi}

Uncertainty in mol-% c_1 due to uncertainty in M_{osp} (i.e. M_{OF}) = 0.42 mol-%

M_{osp}	f_{gsp}	$z_{w c_1}$	
153	0.8891	}	Lab Reported
163	<u>0.8949</u>	<u>67.872</u>	vs $z_{w c_1} = \underline{67.227}$

Generally the lab-reported molar compositions are $\pm 0.25 - 2^+$ mol-% for c_1 and c_{7+}

for various reasons:

GC * $w_i \neq$ BLS (Internal Standard)

* M_i (M_{N+})

* $M_{\bar{o}}$ M_{osp}

* Flash - GC - Recomb : $GOR_F \pm 5\%$

* Sep. (Physical) Recomb : $(GOR_{sp})_{lab} \pm 5\%$

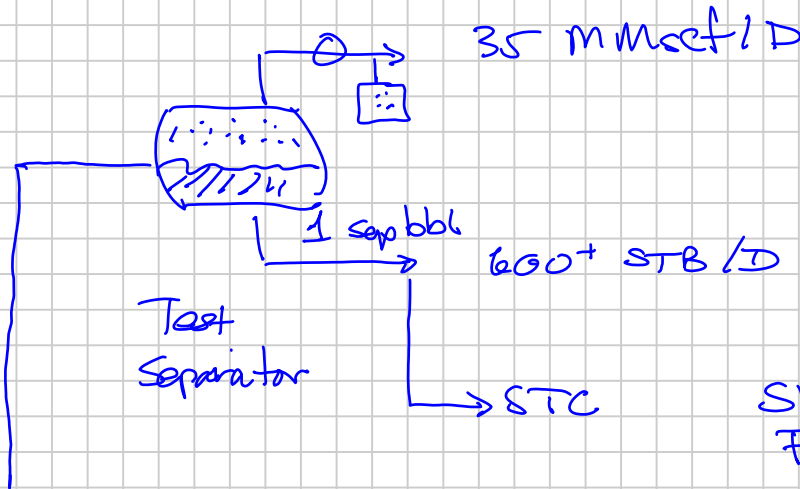
$$\left(\frac{P}{T}\right)_{sp} \approx \left(\frac{P}{T}\right)_{\text{Lab Opening}}$$

$$\frac{138}{(99+460)} = \frac{P_{open}}{(140+460)} \Rightarrow P_{open} \approx 138 \cdot \frac{140+460}{99+460}$$

$$= 148 \text{ psia}$$

$$\text{vs } 155 \text{ psia}$$

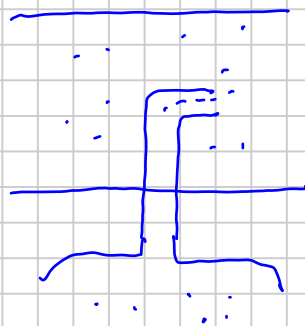
Why would gas bottle to $T > T_{sp}$ be a not good thing? liquid carryover into the gas sample bottle



$$\text{Shrinkage Factor} = \frac{V_o}{V_{osp}}$$

$$= \frac{1}{B_{osp}}$$

Separator Oil Volume Factor



Gas liquids:

y_{spi} 1 Mscf \Rightarrow gallons of i from 1 Mscf

L_i GPM ~~lb/lb mole~~

$$L_i = y_i \cdot \frac{1000 \text{ scf/Mscf}}{379 \text{ scf/lb mole}} \cdot \left(\frac{M_i}{P_{iL}} \right) \cdot \frac{7.48 \text{ gal}}{\cancel{\text{ft}^3}}$$

$\frac{\text{gallons}}{\text{Mscf}}$

$\frac{\cancel{\text{lb}}}{\cancel{\text{ft}^3}}$

$$= \underbrace{y_i \left(\frac{M_i}{P_{iL}} \right)}$$

\$ Condensate

3rd Product

\$ \$

NGH

C_{3+}

C_{4+}

} Liquids extracted from surface gases

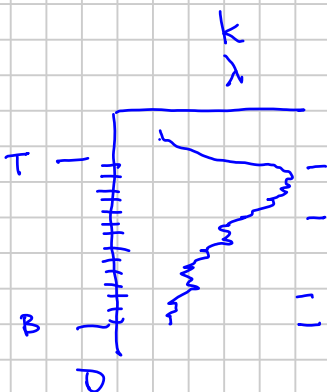
\$ \$ \$

LPG

C_3

C_4

PLT-%



$$\bar{z}_{Ri} = \frac{\int_B^T \lambda(D) z_{Ri}(D) dD}{\int_B^T \lambda(D) dD}$$

SAMPLING

* Types of Sample Methods

① Surface Separator Samples

② Bottomhole Samples



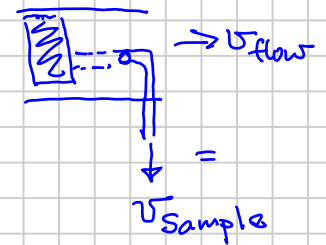
(a) Traditional Cased-hole (wireline) : OILS

(b) Openhole Formation Tester (MDT, RCI, ...):

$z_{Ri} (D)$

③ "Exotic" Samples

(a) Isokinetic Separator Samples
SPE 28829



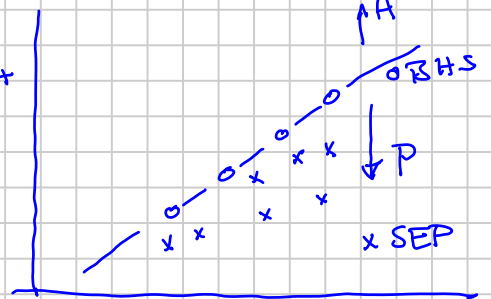
(b) Isokinetic Wellhead Samples

* Special Sampling Issues :

- BHS {
- Waxy fluids ("high" content n-alkanes C_{20+}) = $f(T)$
 - Asphaltenic fluids $p \rightarrow p_s(p)$
max tendency to deposit asphaltene
 - Water
 - Salinity | HC/CO₂ Solubilities (Ch. 9)
 - Oil-Based Mud issues
 - Only Openhole Formation Samples
 - Decantamination of $\gamma_0 \gamma_{7+}$
- (OHF) MDT-type samples.

Excess of these wax-forming compounds in surface samples

$$OHF \quad z_{Si} = z_{Ri} (D) \cdot (1 - f_{obm}) + x_{obmi} \cdot f_{obm}$$



Reservoir Molar OB M Contaminant

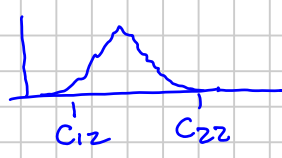
$$f_{obm} \equiv \frac{n_{obm}}{n_{obm} + n_R}$$

N+1 unknowns z_{Ri}, f_{obm}

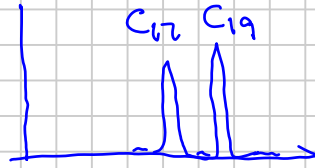
⇒ Very good estimate of z_{Ri} & f_{obm} usually

OBM X_{obmi}

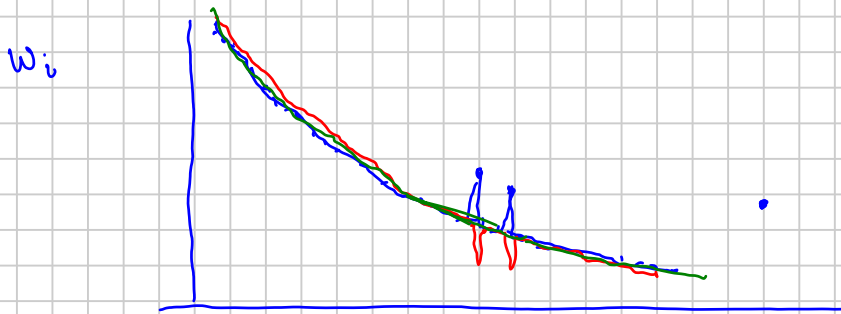
X_{mi}



Distribution in OBM



OHF Z_{Si} : C_{1+} components



$f_{obm}?$

f_{obm} too large

f_{obm} ✓

M_i
SCN

f_{obm}

$$\hat{Z}_{Ri} = (Z_{Si} - f_{obm} X_{mi}) / (1 - f_{obm})$$

C_{1+} of Flashed Oil or Reservoir Fluid

i	Z_{Si}	X_{mi}	\hat{Z}_{Ri}	C_{15} / C_{17}
C_7				
C_8				
\vdots				

OBM: $M_{obm} \sim 200$

16.14 ~ 224

Same basic procedure using Flashed Oil mass fractions with OBM contamination

$$f_{Fobm} = \frac{m_{obm}}{m_{obm} + m_{OF}}$$

GCOBM-report.pdf

$$W_{Fsi} = W_{Si} (1 - f_{Fobm}) + W_{mi} \cdot f_{Fobm}$$

\uparrow Recombine w/ W_{OFi} w/ $(GOR_F^*)_{corr}$

* WHY SAMPLE ?

- II 1. Get an estimate of in-situ reservoir fluid
- I 2. Build EOS model
- II 3. Variation of in-situ fluids spatially
- I 4. Studies on solid (wax/asphaltene) precipitation
- I 5. Build PVT models for pipeflow (T variations)
- II 6. Fluid definition (gas or oil)
- II/I 7. Study fluid heterogeneity / uncertainty analysis
I II I

✓ (I) Build PVT Models All (1) - (4) Data

(II) Map In-Situ Fluid Distribution (2i) (1)

What to do with the samples, once collected ?

- (1) Measure composition
- (2a) Measure $p_s(T)$ / $f(p > p_s)$
- (2b) Multi-stage separator test
- (3) Viscosities
- (4) Two-phase behavior
 - $v_o(p < p_s)$ (a)
 - $v_g(p < p_s)$
 - S_o $p < p_s$ (b)
 - S_g
 - $\{x_i$
 $\{y_i$ $p < p_s$ (c)

$$\checkmark \begin{cases} \mu_o & p < p_s \\ \mu_g & p < p_s \end{cases} \quad (d)$$

$$\sigma_{go} \quad p < p_s \quad (e)$$

⑤ Fill little bottles that we give away

FLUID INITIALIZATION

$z_i (I, J, K)$

① Depth Variations (K)

